

# Lecture 26b: Summary of Availability/Exergy

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# Review Availability and Exergy

□ Mass balance for CV:  $\frac{dm_{CV}}{dt} = \sum_{in} \dot{m}_{in} - \sum_{out} \dot{m}_{out}$   
» For CM:  $m = \text{constant}$

□ Energy balance for CV:

$$\frac{dE_{CV}}{dt} = \dot{Q} + \dot{W} + \sum_{in} \dot{m}_{in} \left( h + \frac{v^2}{2} + gz \right)_{in} - \sum_{out} \dot{m}_{out} \left( h + \frac{v^2}{2} + gz \right)_{out}$$

» For CM:  $dE_{CM} = dU_{CM} + dKE_{CM} + dPE_{CM} = \dot{Q}dt + \dot{W}dt$

□ Entropy Balance for CV:

$$\frac{dS_{CV}}{dt} = \sum_j \frac{\dot{Q}_j}{T_{b,j}} + \sum_{in} \dot{m}_{in} s_{in} - \sum_{out} \dot{m}_{out} s_{out} + \dot{\sigma}$$

» For CM:  $\frac{dS_{CM}}{dt} = \sum_i \frac{\dot{Q}_i}{T_{b,i}} + \dot{\sigma}$

# Review Availability and Exergy

- Availability or non-flow exergy for closed systems:

$$\Phi = m\phi = m[(u - u_0) + P_0(v - v_0) - T_0(s - s_0) + ke + pe]$$

- Relationship between useful work and availability:

$$W_{\text{act,use,tot}} = (E_2 - E_1) + p_0(V_2 - V_1) - T_0(S_2 - S_1) - \sum_j Q_j \left(1 - \frac{T_0}{T_j}\right) + T_0\sigma_{\text{tot}}$$

$$\Rightarrow W_{\text{act,use,tot}} = \Phi_2 - \Phi_1 - \sum_j Q_j \left(1 - \frac{T_0}{T_j}\right) + T_0\sigma_{\text{tot}} \quad T_j = \text{temp. of reservoir}$$

$$\text{or } W_{\text{act,use,CM}} = \Phi_2 - \Phi_1 - \sum_i Q_i \left(1 - \frac{T_0}{T_i}\right) + T_0\sigma_{\text{CM}} \quad T_i = \text{temp. of sys. bound.}$$

# Review Availability and Exergy

- Stream availability or flow exergy:

$$\dot{\Psi} = \dot{m}\psi = \dot{m} \left[ (h - h_o) + \frac{v^2}{2} + g(z - z_o) - T_o(s - s_o) \right]$$

- Exergy balance for CV:

$$\frac{d\Phi_{CV}}{dt} = \sum_{in} \dot{m}_{in} \psi_{in} - \sum_{out} \dot{m}_{out} \psi_{out} + \sum_j \dot{Q}_j \left( 1 - \frac{T_o}{T_j} \right) + \left( \dot{W}_{CV} + p_o \frac{dV_{CV}}{dt} \right) - T_o \dot{\sigma}_{CV}$$

$$\dot{W}_{CV} = \dot{W}_{use} - p_o \frac{dV_{CV}}{dt}$$

- Irreversibilities or exergy destruction

$$\dot{I}_{CV} = T_o \dot{\sigma}_{CV}$$

# Review Availability and Exergy

## □ Heat Engine (power cycle):

» Thermal efficiency (based on First Law):

$$\eta_{\text{thermal,HE}} = \frac{|W_{\text{net}}|}{Q_H} = \frac{|Q_H| - |Q_L|}{|Q_H|} = 1 - \frac{|Q_L|}{Q_H}$$

» Reversible heat engine (Carnot heat engine)

$$\eta_{\text{thermal,HE,rev}} = \eta_{\text{Carnot,HE}} = 1 - \frac{|Q_L|}{|Q_H|} = 1 - \frac{T_L |\Delta S_L|}{T_H |\Delta S_H|} = 1 - \frac{T_L}{T_H}$$

» Second Law efficiency/effectiveness

– For reservoirs:

$$\varepsilon_{\text{II,HE}} = \eta_{\text{II,HE}} = \frac{\eta_{\text{thermal,HE}}}{\eta_{\text{Carnot,HE}}} = \frac{|\dot{W}_{\text{out,use}}|}{\dot{\Phi}_{Q_H}} = \frac{\eta_{\text{th,act}} |\dot{Q}_H|}{|\dot{Q}_H| \underbrace{\left(1 - \frac{T_0}{T_H}\right)}_{=\eta_{\text{th,Carnot}}}}$$

– Finite temperatures:

$$\varepsilon_{\text{II,HE}} = \eta_{\text{II,HE}} = \frac{|\dot{W}_{\text{out,use}}|}{\Delta \dot{\Psi}_H}$$

# Review Availability and Exergy

## □ Heat Pump (Air-conditioning/Refrigeration):

» Coefficient of Performance (cooling mode C):

$$COP_{C,act} = \frac{|\dot{Q}_L|}{\dot{W}}$$

» Reversible heat pump cycle (cooling mode)

$$COP_{C,carnot} = \frac{T_L}{T_H - T_L}$$

» Second Law efficiency/effectiveness

– For reservoirs:

$$\varepsilon_{HP,C} = \frac{COP_{C,act}}{COP_{C,carnot}} = \frac{\dot{\Phi}_{Q_L}}{\dot{W}}$$

– General expression:

$$\varepsilon_{HP,C} = \frac{COP_{C,act}}{COP_{C,carnot}}$$

# Review Availability and Exergy

## □ Heat Pump (Heating):

» Coefficient of Performance (heating mode H):

$$COP_{H,act} = \frac{|\dot{Q}_H|}{\dot{W}}$$

» Reversible heat pump cycle (heating mode)

$$COP_{H,Carnot} = \frac{T_H}{T_H - T_L}$$

» Second Law efficiency/effectiveness

– For reservoirs:

$$\varepsilon_{HP,H} = \frac{COP_{H,act}}{COP_{H,Carnot}} = \frac{\dot{\Phi}_{Q_H}}{\dot{W}}$$

– General expression:

$$\varepsilon_{HP,H} = \frac{COP_{H,act}}{COP_{H,Carnot}}$$

# Review Availability and Exergy

## □ Turbine (adiabatic):

» Isentropic efficiency:

$$\eta_{t,is} = \frac{|w_{\text{actual}}|}{|w_{\text{isentropic}}|}$$

» Exergetic efficiency/effectiveness

$$\varepsilon_t = \frac{|\dot{W}_{\text{actual}}|/\dot{m}}{\psi_{in} - \psi_{out}}$$

## □ Compressor/Pump (adiabatic):

» Isentropic efficiency:

$$\eta_{c,is} = \frac{w_{\text{isentropic}}}{w_{\text{actual}}}$$

» Exergetic efficiency/effectiveness:

$$\varepsilon_t = \frac{\psi_{out} - \psi_{in}}{\dot{W}_{\text{actual}}/\dot{m}}$$



# Review Availability and Exergy

- Heat exchanger without mixing and adiabatic (c=cold stream; h=hot stream):
  - » Exergetic efficiency/effectiveness

$$\varepsilon_{HX} = \frac{\dot{m}_c(\psi_{c,out} - \psi_{c,in})}{\dot{m}_h(\psi_{h,in} - \psi_{h,out})}$$

- Direct contact heat exchanger (mixing) adiabatic:
  - » Hot stream: 1
  - » Cold stream: 2
  - » Mixed stream: 3

$$\varepsilon_{mix} = \frac{\dot{m}_2(\psi_3 - \psi_2)}{\dot{m}_1(\psi_1 - \psi_3)}$$

- General definition of second law efficiency/effectiveness:

$$\varepsilon_{II} = \frac{\text{Exergy recovered}}{\text{Exergy supplied}} = 1 - \frac{\text{Exergy destroyed}}{\text{Exergy supplied}}$$